

Effect of ultrasound radiation on the size and size distribution of synthesized copper particles

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Abstract The effect of ultrasound radiation on the size and size distribution of synthesized copper particles was investigated under various concentrations of ethylene glycol (E.G.) as a capping agent. Monodispersed copper particles were produced by the reduction of an aqueous copper (II) sulfate solution at the presence of hydrazine monohydrate. X-ray diffraction and scanning electron microscopy analysis revealed that the morphology, size, and size distribution of produced particles were influenced by the reducing agent injection rate, capping agent concentration, and sonication. Increasing the injection rate of reducing agent to an amount higher than a critical value decreases the size of copper particles and also converts the monodispersed particles to polydispersed particles. Results of using a sonifier at the reduction stage revealed that finer monodispersed copper particles can be achieved at higher injection rates related to the critical value. Increasing the concentration of E.G. as a capping agent decreases the size of copper particles, while applying ultrasound radiation along with increasing the concentration of E.G. increases the size of copper particles. Morphology of particles varies by the concentration and type of the capping agent. Higher reducing agent injection rates and the application of a sonifier at the instance of reduction result in smaller spherical particles at various capping agent concentrations.

Introduction

In recent years, much attention has been paid to metal nano-particles due to their novel optical, electronic, magnetic, and chemical properties resulting from their extremely small dimensions and special surface [1–5]. Among various metal particles, copper nano-particles have attracted considerable attention because of their superior thermal and electrical conductivity. Different methods have been developed for the preparation of copper nano-particles including micro emulsion techniques [6–8], laser ablation [9], radiation methods [10], wet chemical reduction [11], thermal reduction [5], metal vapor synthesis [12], and vacuum vapor deposition [13]. The wet chemical reduction method has been widely used by many researchers because of its superior ability in controlling the size and morphology of nano-particles for large-scale production. Organic solvents such as ethylene glycol (E.G.) [14], *n*-heptane, *n*-octane, *n*-hexane, cyclohexane, CHCl₃ [15], benzene, toluene [16] and organic capping agents such as poly(vinylpyrrolidone) [14], sodium dodecyl sulfate [17], hexadecyltrimethylammonium bromide [18], octadecylamine [19], ethylene diamine [20] are the most common reactants used in wet chemical method. In the reported studies, the reaction solutions were carefully deoxygenated and the processes were performed under a rigorous protection of inert gas to prevent the oxidation. Wu and Chen independently reported the synthesis of copper nano-particles in an aqueous system under a nitrogen atmosphere [18]. Kumar et al. and Dhas et al. prepared copper nano-particles by using the sono-chemical reduction method. Their product was a mixture of copper and copper oxide nano-particles [21, 22]. In sono-chemistry the main event is the creation, growth, and collapse of a bubble that is formed in the liquid. Each collapsing bubble forms a few nucleation

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centers whose growth is limited by the short collapse [22]. In most of these studies, organic solvents [14–16, 23], capping agents [17–20], high temperature [24], inert atmospheres [18, 21], and a limited injection rate of the reducing agent [14] have been used to control the size, distribution, and purity of synthesized copper particles. Removing the used organic solvent and capping agent under controlled atmosphere needs a tedious procedure which is time consuming and expensive.

In the present work, ultrasound radiation has been used to produce monodispersed metallic copper particles in an aqueous solution without any copper oxide by product at ambient atmosphere. The effect of ultrasound radiation and injection rate of reducing agent on the size and size distribution of synthesized copper particles was investigated under various concentrations of E.G. as a capping agent. One of the most important advantages of ultrasound radiation is that smaller spherical monodispersed copper particles can be produced at high reducing agent injection rates and high concentration of copper ions. This method can be useful for large-scale production of monodispersed copper particles.

Materials and methods

Materials and synthesis

All reagents used in this work were analytical grade, including ethylene glycol (E.G., $C_2H_6O_2$, $M_w = 62.078$, 99.5%, Carlo Erba) as a protecting agent, hydrazine monohydrate (N_2H_5OH , %80, $M_w = 50$, 80%, Merck) as a reducing agent and copper (II) sulfate anhydrous ($CuSO_4$, $M_w = 159.61$, Merck) as a copper source. Copper particles were obtained by adding hydrazine monohydrate to the aqueous solution of copper (II) sulfate and E.G. at ambient atmosphere. In a typical preparation of copper particles,

20 mL of an aqueous solution containing 0.32 g (2 mmol) $CuSO_4$ and various amounts of E.G. at 60 °C (Table 1) was titrated by NaOH until pH = 4 was reached. Then a 5 mL aqueous solution containing 0.5 mL hydrazine hydrate (80%) was added in various injection rates under ultrasound radiation (Table 1). The synthesized copper particles were recovered from the solution by centrifuging which was subsequently washed repeatedly with distilled water and dried in an oven. X-ray diffraction technique employing $Cu K_{\alpha 1}$ radiation (1.51059 Å) was used to characterize the composition and crystallinity of synthesized particles. Scanning electron microscopy was employed to reveal the morphology, size, and size distribution of the prepared copper particles.

Characterization of copper nano-particles

In addition to the particle size and size distribution, phase composition and crystallinity of the synthesized copper particles were investigated by using an X-ray diffractometer. The phase analysis was conducted on the monodispersed copper particles (sample #6). The X-ray diffraction patterns correspond to copper with a crystalline face-centered-cubic (fcc) structure as shown in Fig. 1. The prepared particles were determined to be pure Cu without any impurity such as CuO , Cu_2O , and $Cu(OH)_2$. Size and size distribution of synthesized copper particles were determined with Microstructure Measurement software.

Results and discussion

Basic chemical reaction

Typically, during titration of the sodium hydroxide solution, copper (II) sulfate converts to copper hydroxide [$Cu(OH)_2$] followed by the formation of cuprous oxide

Table 1 Synthesis parameters of prepared copper particles

Sample ID	Protecting agent	Protecting agent (mmol)	Injection rate of reluctant (mL/min)	Ultrasound radiation
#1	—	—	0.035	No
#2	—	—	0.083	No
#3	—	—	60	No
#4	E.G.	1	60	No
#5	E.G.	—	60	Yes
#6	E.G.	1	60	Yes
#7	E.G.	2	60	Yes
#8	E.G.	4	60	Yes
#9	E.G.	6	60	Yes
#10	E.G.	8	60	Yes
#11	E.G.	10	60	Yes

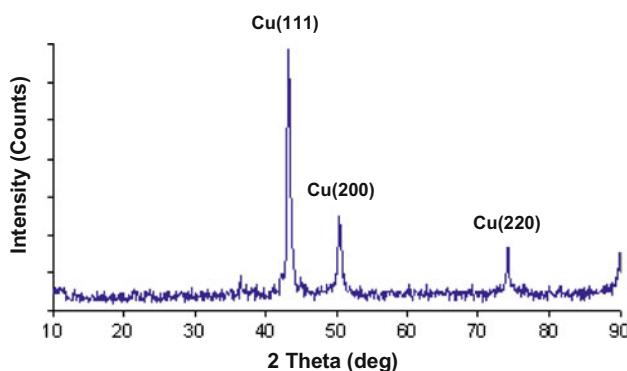


Fig. 1 X-ray diffraction of synthesized copper particles (sample #6)

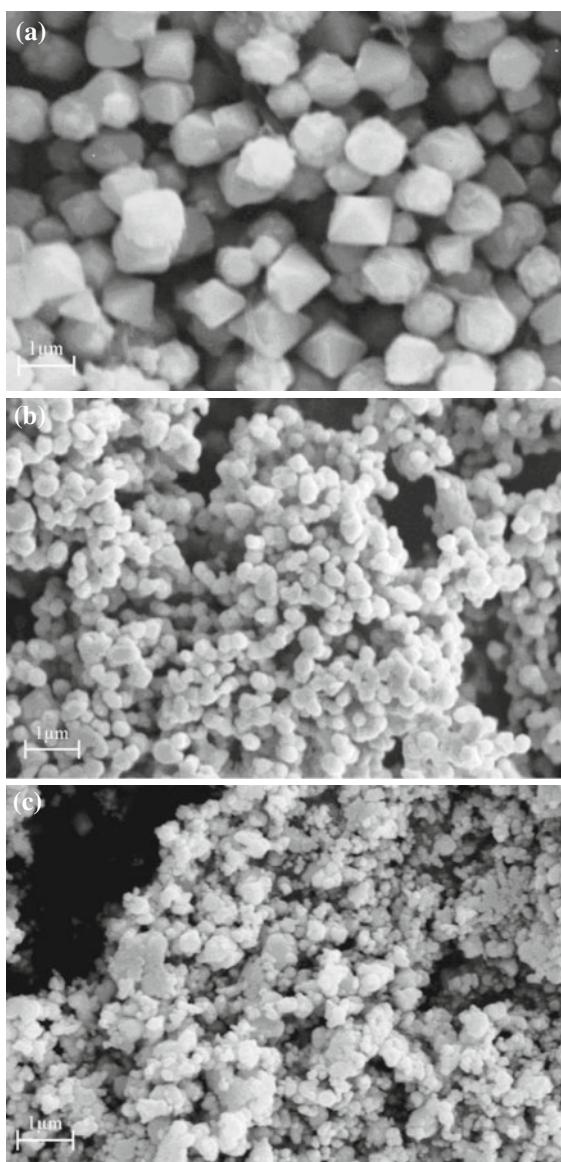
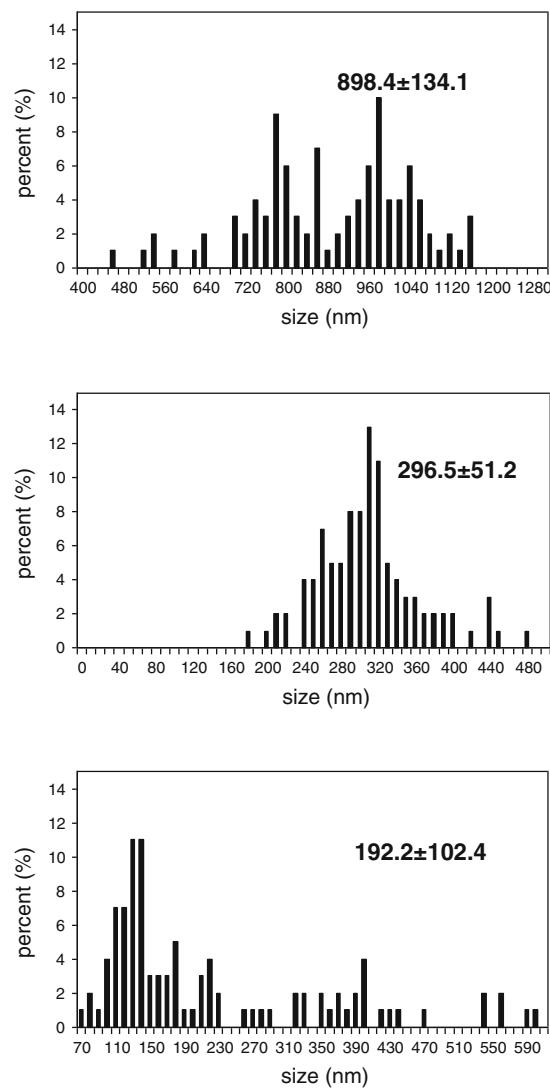


Fig. 2 SEM images of synthesized copper particles at various injection rates of reducing agent. **a** 0.035 mL/min, average particles size 898.4 ± 134.1 nm (sample #1); **b** 0.083 mL/min, average

(Cu_2O) as an intermediate product which forms copper as the final product according to the following equation [25]:
 $\text{Cu}(\text{OH})_2 \rightarrow \text{Cu}_2\text{O} \rightarrow \text{Cu}$

Effect of the reducing agent injection rate

Three different injection rates (Table 1) were selected to prepare copper particles at 60 °C. Figure 2 shows the SEM images of synthesized copper particles for different injection rates of the reducing agent. At an injection rate of 0.035 mL/min the average diameter of obtained particles is 898.4 ± 134.1 nm (Fig. 2a). By increasing the injection



particles size 296.5 ± 51.2 nm (sample #2); **c** 60 mL/min, average particles size 192.2 ± 102.4 nm (sample #3)

rate to 0.083 mL/min, smaller particles (296.5 ± 51.2 nm) were obtained with a narrow size distribution but the shape of the particles changed from octahedral and polyhedral type with distinct faces of {111} to a spherical shape (Fig. 2b). Figure 2c shows that a further increase in the injection rate (60 mL/min) results in finer particles with a broader size distribution and the shape of particles changed to irregular shape (192.2 ± 102.4 nm).

The size and size distribution of the obtained particles are determined by the nucleation and the growth mechanisms. The formation of nuclei needs a critical concentration of reduced copper atoms, C_{crit} . The time to reach C_{crit} (Incubation Time (I.T.)) depends on the concentration of reduced copper atoms which is affected by injection rate of the reducing agent, degree of homogenization, and concentration of copper ions. By increasing the injection rate of reducing agent the incubation time will be decreased and also the reduction rate of copper ions exceeds the consumption rate of copper atoms in the growth mechanism. Consequently, the concentration of reduced copper atoms ($C_{\text{saturation}}$) remains over C_{crit} for longer times or fluctuates around it [23] which results in renewed nucleation and polydispersed particles during the reaction (Fig. 4b).

Influence of sonication on the size and size distribution of particles

The effect of sonication on the size and size distribution of particles is described in this section. By employing ultrasound radiation the average diameter of synthesized copper particles decreases from 253.4 ± 74.3 nm (Fig. 3a) to 112.8 ± 19.1 nm (Fig. 3b) by employing ultrasound radiation. These results showed that application of ultrasound radiation results in smaller monodispersed particles compared to the case without using any sonication.

Because of the low dispersibility of the stirrer compared to the ultrasound probe in dispersing reducing agents and reducing copper atoms at high injection rate, local nucleation occurs around the droplet of the reducing agent. This local nucleation increases the local $C_{\text{Saturation}}$ and decreases the I.T. around the droplet of the reducing agent. Ultrasound radiation uniformly distributes the reductant through the reaction mixture which decreases the local volumetric concentration ($C_{\text{Saturation}}$) of the reduced copper atoms in compared to the case without using sonication. According to the LaMer diagram, the concentration of copper atoms ($C_{\text{Saturation}}$) which is controlled by reducing agent injection rate, degree of homogenization, and concentration of

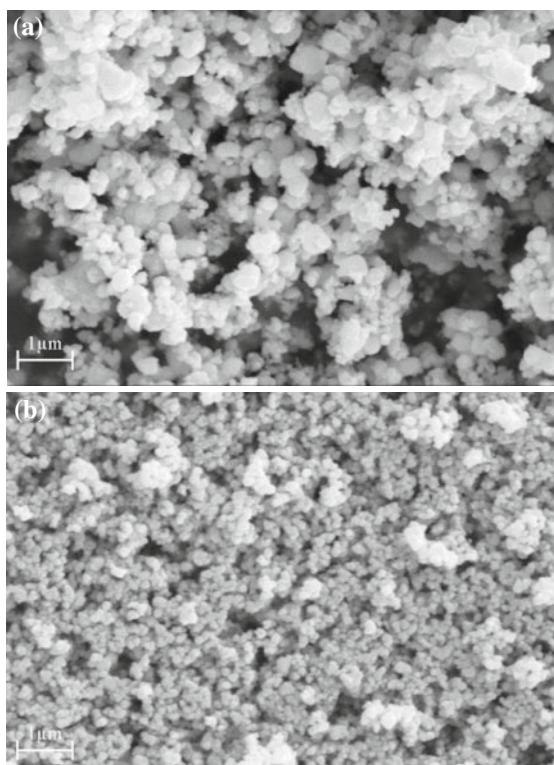
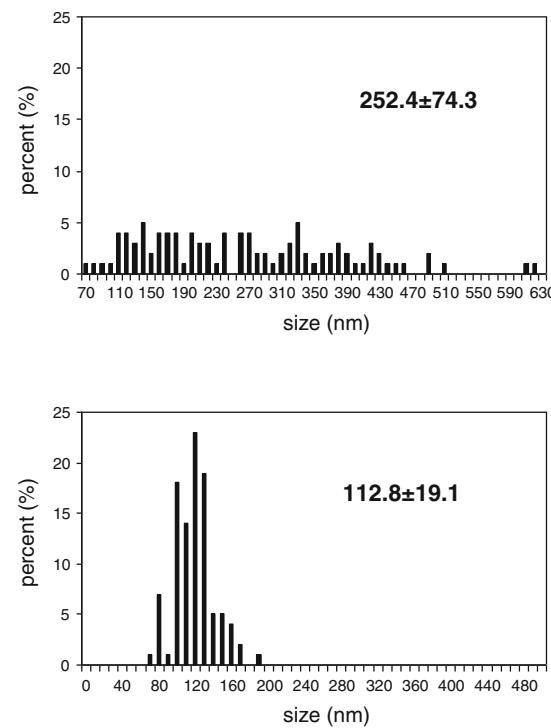


Fig. 3 SEM images of synthesized copper particles. **a** Average particles size 253.4 ± 74.3 nm (sample #4) without using ultrasound radiation. **b** Average particles size 112.8 ± 19.1 nm (sample #6) with using ultrasound radiation



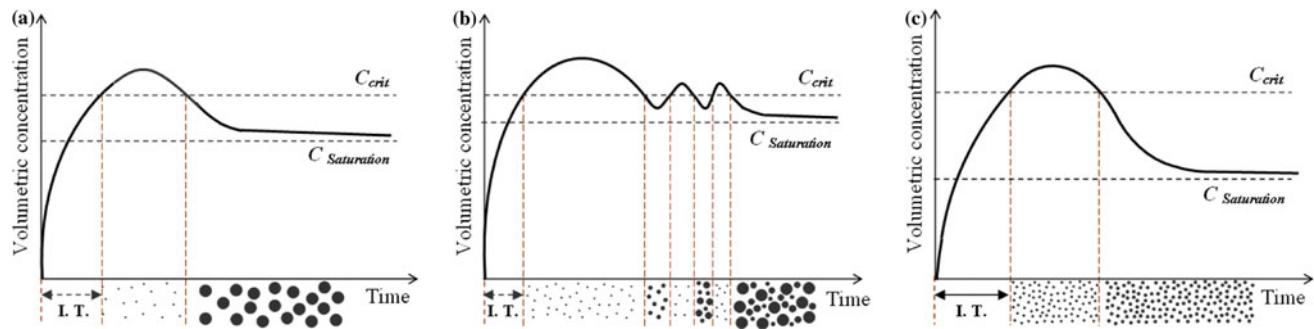


Fig. 4 Schematic representation of size and size distribution of synthesized particles at **a** low injection rate, **b** high injection rate of the reducing agent [23], and **c** with using ultrasound radiation at high

injection rate. $((I.T.)_b < (I.T.)_c$ and $(C_{saturation})_b > (C_{saturation})_c$). Increasing the I.T. and decreasing the $C_{saturation}$ under ultrasound radiation results in monodispersed particles

copper ions determines the size and size distribution of particles. Therefore, in experimental condition, the stage to reach polydispersed particles can be controlled by injection rate, degree of homogenization, and concentration of copper ions. Decreasing the local concentration of copper atoms retards the nucleation stage and consequently increases the incubation time and the number of nuclei (Fig. 4c). When the concentration reaches to C_{crit} , due to the uniform distribution of copper atoms more nuclei form at a short time decreasing the amount of available copper atoms for particle growth per growing particle. Decreasing the amount of available copper atoms ($C_{saturation}$) for particle growth rapidly drops the volumetric concentration under C_{crit} and stops the nucleation period finally resulting in monodispersed copper particles. After the growth of nucleus starts, smaller particles will be produced due to the large number of nuclei and the lower amount of available copper atoms for growth. Eventually, using high injection rate condition at the presence of the ultrasound radiation produces smaller particles with a narrower size distribution (Fig. 4c).

Effect of E.G. concentration as a capping agent

The effect of E.G. concentration on the size and size distribution of particles is described in this section. Ahmadi et al. [26] reported that the size and morphology of Pt particles can be controlled by changing the concentration ratio of capping agent (sodium polyacrylate) to Pt ions. They claimed that the presence of capping agent is believed to have two functions. First, it stops the growth of particles at a small size distribution. Second, it prevents individual colloidal particles to coalescence with each other [26]. Herein the influence of the concentration ratio of E.G. to copper ions on the size and size distribution of copper nano-particles was investigated at the presence of ultrasound radiation. Results show that under ultrasound

radiation larger spherical particles were obtained by increasing the concentration ratio of E.G. to copper ions (Fig. 5). We believe that copper ions are covered by E.G. molecules and this layer decreases the reduction rate of copper ion–E.G. structure which inevitably increases the incubation time for copper atoms to reach C_{crit} . Therefore, the nucleation rate of copper particles will be decreased by increasing the concentration of the capping agent (E.G.). Decreasing the nucleation rate elevates the growth rate resulting in larger copper particles. Increasing the concentration of capping agent not only results in larger particles, but also affects on the size distribution of the synthesized particles (Fig. 5). Variation of the average particle size and standard deviation versus concentration ratio of capping agent to copper source has been illustrated in Fig. 6a and b. As it can be seen, the average particle size, increases from 108 to 185 nm at the first interval (samples 5, 6, 7, and 8) and remains constant with a slight variation between 185 and 200 nm at the second interval (samples 8, 9, and 10) and again sharply increases from 200 to 300 nm at the third interval (samples 10 and 11). The increase in the average particle size at these three different intervals are 20, 3.5, and 50 nm per 1 mmol of E.G., respectively. Figure 6b depicts the standard deviation curve in which the maximum standard deviation at sample #10 (8 mmol of E.G.) related to a drop in average size at Fig. 6a. Increase in the average size and decrease in the standard deviation at definite concentrations of E.G. can be related to the amount of E.G. that cover the copper ions. With increasing the amount of E.G. some copper ions (but not all ions) are covered by E.G. causing an increase in the average size and due to unequal distribution of E.G. for copper ions the standard deviation increases. When the concentration of E.G. increases up to definite level, all the copper ions are equally covered by E.G. causing an increase in size of all particles with narrower standard deviation.

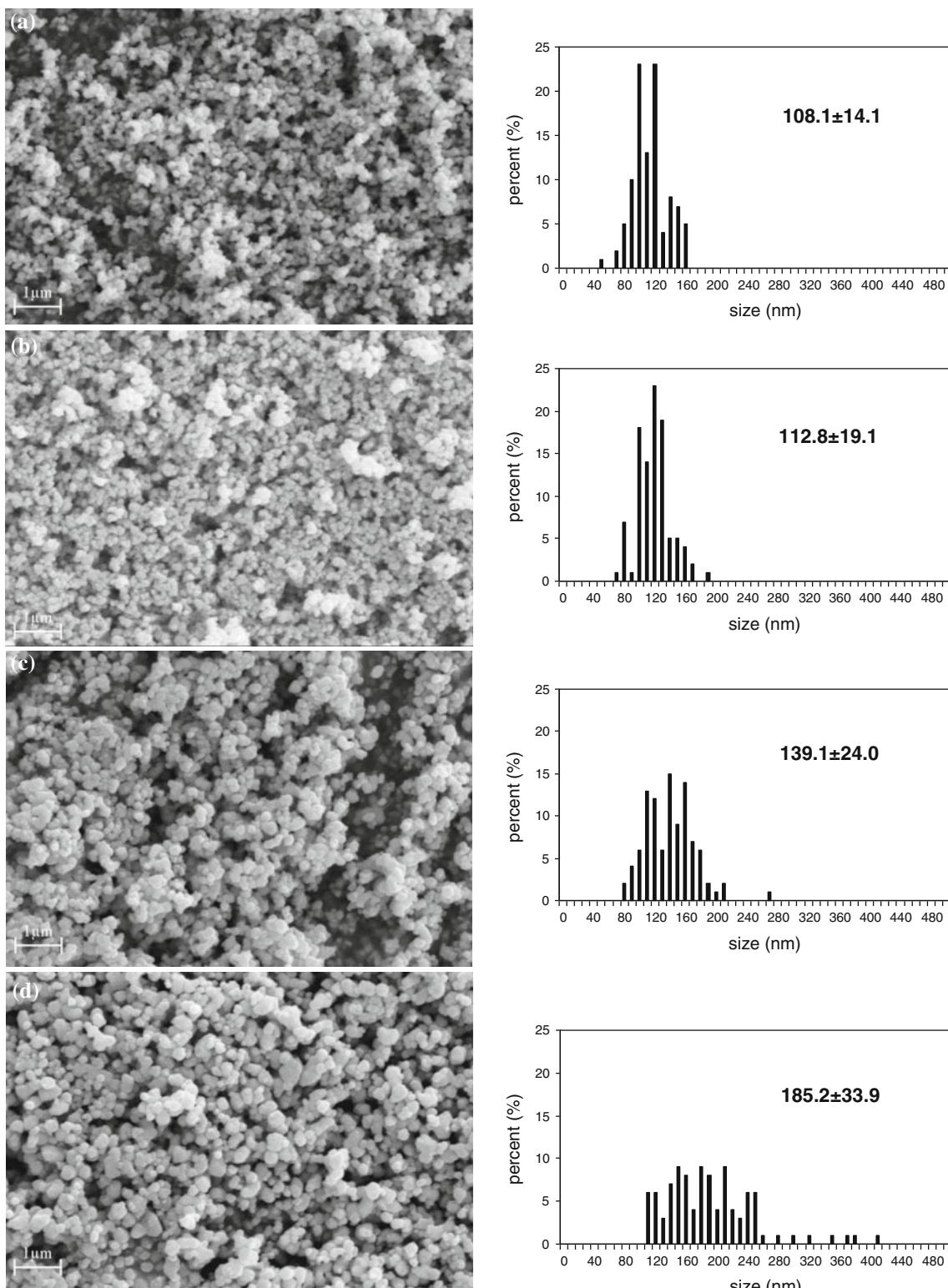


Fig. 5 SEM images of synthesized copper particles in various amounts of E.G. and size distribution diagrams. **a** 0 mmol, 108.1 ± 14.1 nm (sample #5); **b** 1 mmol, 112.8 ± 19.1 nm (sample #6); **c** 2 mmol, 139.1 ± 24.0 nm (sample #7); **d** 4 mmol, 185.2 ± 33.9 nm (sample #8); **e** 6 mmol, 201.7 ± 49.3 nm (sample #9); **f** 8 mmol, 189.5 ± 59.7 nm (sample #10); and **g** 10 mmol, 300.2 ± 52.7 nm (sample #11)

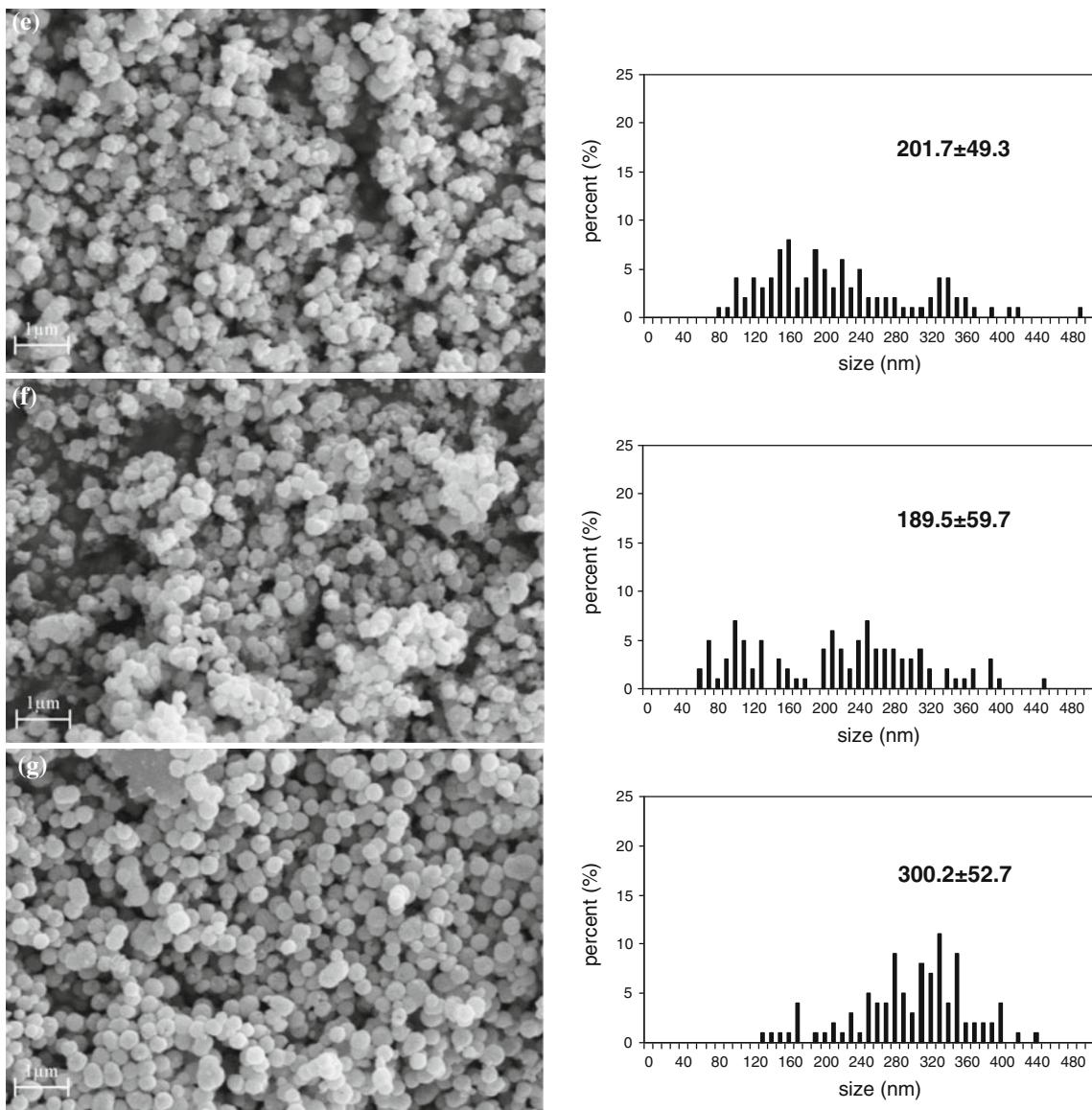


Fig. 5 continued

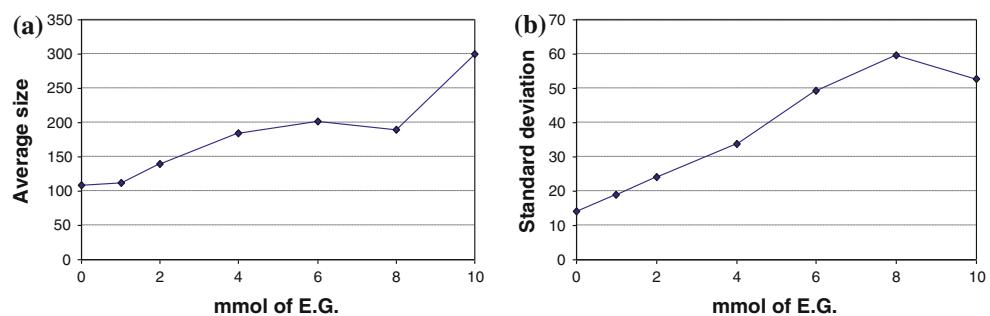


Fig. 6 The average size and standard deviation of synthesized copper particles in various concentration of E.G. **a** Average size, **b** standard deviation

Conclusion

We synthesized high pure monodispersed copper nano-particles via a wet chemical route. Results show that increasing the injection rate of reducing agent decreases the size of copper particles and also converts the monodispersed particles to polydispersed form and also affect the particle shape. Monodispersed copper nano-particles with average diameter around 108 nm were obtained by applying ultrasound radiation at higher injection rates of the reducing agent and the concentrated solution. We showed that the concentration ratio of E.G. to copper ions is a key factor in controlling the size of copper nano-particles. Increasing the concentration of E.G. increases the mean diameter of synthesized copper nano-particles. Unlike the polyol method which uses E.G. as solvent, we showed that high pure spherical and monodispersed copper nano-particles can be produced in water at large scale.

References

1. Gates BC (1995) *Chem Rev* 95:511
2. Schmid G (1992) *Chem Rev* 92:1709
3. Kamat PV (1993) *Chem Rev* 93:267
4. Alivisatos AP (1996) *J Phys Chem* 100:13226
5. Beecraft LL, Ober CK (1997) *Chem Mater* 9:1302
6. Lisiecki I, Pileni MP (1993) *J Am Chem Soc* 115:3887
7. Pileni MP, Nilham BW, Gulik-Krzywicki T, Tanori J, Lisiecki I, Filankembo A (1999) *Adv Mater* 11:1358
8. Qi L, Ma J, Shen J (1997) *J Colloid Interface Sci* 186:498
9. Yeh MS, Yang YS, Lee YP, Lee HF, Yeh YH, Yeh CS (1999) *J Phys Chem B* 103:6851
10. Casella IG, Cataldi TRI, Guerrieri A, Desimoni E (1996) *Anal Chim Acta* 335:217
11. Huang HH, Yan FQ, Kek YM, Chew CH, Xu GQ, Ji W, Oh PS, Tang SH (1997) *Langmuir* 13:172
12. Vitulli G, Bernini M, Bertozzi S, Pitzalis E, Salvadori P, Coluccia S, Martra G (2002) *Chem Mater* 14:1183
13. Liu Z, Bando Y (2003) *Adv Mater* 15:303
14. Park BK, Jeong S, Kim D, Moon J, Lim S, Kim JS (2007) *J Colloid Interface Sci* 311:417
15. Song X, Sun S, Zhang W, Yin Z (2004) *J Colloid Interface Sci* 273:463
16. Liu W, Wang X, Fu S (2006) US Patent 0053927
17. Lisiecki I, Billoudet F, Pileni MP (1996) *J Phys Chem* 100:4160
18. Wu SH, Chen DH (2004) *J Colloid Interface Sci* 273:165
19. Shi Y, Li H, Chen L, Huang X (2005) *Sci Technol Adv Mater* 6:761
20. Chang Y, Lye ML, Zeng HC (2005) *Langmuir* 21:3746
21. Kumar RV, Mastai Y, Diamant Y, Gedanken A (2001) *J Mater Chem* 11:1209
22. Dhas NA, Raj CP, Gedanken A (1998) *Chem Mater* 10:1446
23. LaMar VK, Dinegar RH (1950) *J Am Chem Soc* 72:4847
24. Kim JS, Moon JH, Jeong SH, Kim DJ, Park BK (2007) US Patent 0180954
25. Miki H (1998) US Patent 5741347
26. Ahmadi TS, Wang ZL, Green TC, Henglein A, El-Sayed MA (1996) *Science* 272:1924